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㉛ Process for the production of chlorine.

㉜ Chlorine can be efficiently produced at a low temperature and at a high rate by oxidizing hydrogen chloride with an oxygen-containing gas in the presence of a catalyst comprising a compound obtained by reacting chromium nitrate, chromium chloride, the chromium salt of an organic acid or the like with ammonia. The compound, or a mixture of the compound and a silicon compound, may be calcined, preferably at a temperature lower than 800°C.

PROCESS FOR THE PRODUCTION OF CHLORINE

This invention relates to an improved process for producing chlorine by oxidizing hydrogen chloride with an oxygen-containing gas in the presence of a catalyst at a low temperature and in a gas phase.

Chlorine is produced on large scales by the electrolysis of sodium chloride. In spite of the ever-increasing demand for chlorine, the demand for caustic soda which occurs simultaneously upon the electrolysis of sodium chloride is lower than that for chlorine. Difficulties have thus been encountered in meeting their different demands appropriately.

On the other hand, a great deal of hydrogen chloride is byproduced in the chlorination or phosgenation reaction of an organic compound. Since the volume of such byproduced hydrogen chloride is significantly higher than the demand level for hydrochloric acid, lots of hydrogen chloride is disposed of wastefully without its utilization.

Furthermore, the treatment cost for its disposal has reached a considerable value.

It is thus possible to meet the demand for chlorine without developing an imbalance between its production level and that of caustic soda, provided that chlorine can be efficiently recovered from hydrogen chloride which is disposed of in a large volume as described above.

10 The reaction in which hydrogen chloride is oxidized to produce chlorine has been known as the Deacon reaction for many years. The copper-base catalysts which Deacon invented in 1868 have conventionally been considered to show the best 15 activities. A number of proposals have been made on catalysts which contain various compounds added as a third component to copper chloride and potassium chloride. In order to oxidize hydrogen chloride at an industrially-satisfactory reaction velocity with these 20 catalysts, it is however necessary to raise the reaction temperature to 450°C or higher. At such high reaction temperatures, a problem arises that their catalytic service life is shortened due to scattering of their catalyst components. In addition, the 25 oxidation reaction of hydrogen chloride has an equilibrium point. The yield of chlorine decreases as

the temperature goes up. It is thus required to develop a catalyst which can show its activities at a temperature as low as possible.

From the above-described viewpoint, iron-base catalysts and some other catalysts have been proposed as catalysts other than copper-base catalysts. However, the present inventors are still not aware of any catalysts which may exhibit fully practical quality and performance. It has also been proposed to employ chromium oxide as a catalyst for the oxidation of hydrogen chloride because chromium oxide has better stability and durability at elevated temperatures than copper and the like. As far as the present inventors are aware of, none of such chromium oxide catalysts have yet been reported to have shown satisfactory activities. For example, it is disclosed in U.K. Patent Specification No. 584,790 that hydrogen chloride is caused to flow at about 400°C over a catalyst, which has been prepared by impregnating a suitable carrier with chromic anhydride or an aqueous solution of chromium nitrate and then subjecting the thus-impregnated carrier to pyrolysis, to produce chlorine; and after deactivation of the catalyst, the supply of hydrogen chloride is cut off and air is in turn caused to flow so as to regenerate the catalyst, and the supply of air is then stopped and the supply of

hydrogen chloride is instead resumed. In U.K. Patent Specification No. 676,667, hydrogen chloride and an oxygen-containing gas were reacted at 420 - 430°C in the presence of a catalyst composed of a carrier and a bichromate or heavily dark green chromium oxide supported on the carrier, whereby hydrogen chloride conversions of 67.4% and 63%, both based on the equilibrium value, were achieved at hourly space velocities of 380 hr^{-1} and 680 hr^{-1} respectively.

10 The occurrence of the reaction was still observed at 340°C. However, the hourly space velocity was controlled at such a low level as 65 hr^{-1} and the resultant conversion was as low as 52%.

As mentioned above, even when chromium oxide is used as a catalyst, it is not of such quality that it can withstand an industrial operation because the reaction temperature is high and the hourly space velocity is low in each of such conventional processes. In other words, the chromium oxide catalysts which have conventionally been reported are not believed to exhibit any specifically excellent performance compared with the copper-base catalysts.

20 It is desirable to provide a process for recovering chlorine from hydrogen chloride with good efficiency by using a catalyst which is active at low temperatures and permits the oxidation of hydrogen chloride at a large volume rate.

The present inventors have carried out various researches on the production process of chlorine by the oxidation of hydrogen chloride, especially, on catalysts useful in the oxidation of hydrogen chloride.

5 As a result, it has been found that chlorine can be produced from hydrogen chloride at a higher rate and with a conversion significantly higher than those achieved by conventional processes when a chromium oxide catalyst prepared in accordance
10 with a process, which has not been reported to date with respect to the oxidation of hydrogen chloride, is used.

In one aspect of this invention, there is thus
15 provided a process for producing chlorine by oxidizing hydrogen chloride with an oxygen-containing gas, which comprises effecting the oxidation in the presence of a catalyst prepared from a chromium compound which has been obtained by reacting chromium nitrate, chromium
20 chloride or the chromium salt of an organic acid with ammonia.

In another aspect of this invention, there is also provided a process for producing chlorine by oxidizing hydrogen chloride with an oxygen-containing gas, which comprises effecting the oxidation in the presence of a catalyst prepared from a chromium compound, which has been obtained by reacting a chromium salt with ammonia, and a silicon compound.

5 The catalyst may preferably be used after calcining same at a temperature lower than 800°C.

10 As mentioned above, the present invention makes it possible to produce chlorine from hydrogen chloride at a rate and with a conversion which are significantly higher than those available by conventional processes.

15 The invention also includes the novel catalysts as herein defined.

As hydrogen chloride useful as a raw material in the practice of the process of this invention, it is generally possible to make wide use of byproduced hydrochloric acid such as that byproduced upon chlorination of organic compounds or that byproduced by the reaction between phosgene and organic compounds.

20 The oxygen-containing gas is used as an oxidizing agent for hydrogen chloride. Oxygen gas or air may be used in many instances. Oxygen gas may 25 preferably used where the reactor is of the fluidized

bed type, whereas air may favorably be used where the reactor is of the fixed bed type. As the molar ratio of hydrogen chloride to the oxygen in an oxygen-containing gas, which are both to be fed for the reaction, 5 the oxygen is preferably used in an amount of about 1/4 mole (equivalent) or so per mole of hydrogen chloride. In many instances, oxygen is generally used 5% - 200% in excess of its equivalent. It is suitable to feed hydrochloric acid to a catalyst bed at a flow rate in 10 the range of 200 - 1800 Nl/hr·kgCat. As the reaction temperature, 300 - 400°C or particularly 330 - 390°C are employed frequently. A pressure range of from normal pressure or so to 1 - 10 kg/cm²G is often used as the reaction pressure. The conversion of hydrogen 15 chloride increases as the pressure becomes higher.

The catalyst useful in the practice of the process of this invention is obtained from a chromium compound which has been formed by reacting a chromium salt, which was obtained through the reaction between chromium nitrate, chromium chloride, the chromium salt of an organic acid or chromic anhydride and hydrogen chloride, with ammonia. It is preferred to calcine the chromium compound at a temperature lower than 800°C prior to its application. Alternatively, the catalyst 20 may also be prepared from the above-described chromium compound, which has been obtained by reacting the 25

chromium salt with ammonia, and a silicon compound. It is preferable to calcine the mixture of the chromium compound and silicon compound at a temperature lower than 800°C.

5 The chromium compound can usually be formed by reacting an aqueous solution of the above-described chromium salt with aqueous ammonia. It may also be feasible to use an ammonia-releasing compound, such as urea, in place of ammonia. Generally, the amounts of such chromium salts in water fall in the range of 3 - 10 30 wt.%. It is usually suitable to use aqueous ammonia the NH_4OH concentration of which ranges from 5% to 15 30%. The resulting precipitate is collected by filtration, washed and then dried. Thereafter, it is preferably calcined at a temperature lower than 800°C for several to 20 hours or so in an air atmosphere, in 20 vacuo or in an inert gas atmosphere such as nitrogen gas atmosphere to obtain a catalyst. After the calcination, the resultant catalyst is shaped by the 25 tableting or extrusion method so that it can be used in a fixed-bed reactor. To prepare a catalyst suitable for use in a fluidized bed, the resultant precipitate is washed by decantation and is then converted into a slurry of a suitable concentration. In a spray drier, the slurry is formed into particles and then dried 25 there. Thereafter, the thus-obtained particles are

preferably calcined at a temperature lower than 800°C to obtain a catalyst.

It is essential to use chromium nitrate, chromium chloride, the chromium salt of an organic acid, or a salt which is obtained by the reaction of chromic anhydride and hydrogen chloride, as the starting material for the chromium compound employed in the process of this invention. It is also an essential requirement to use ammonia as an alkaline material for allowing the precipitate to occur.

When chromium sulfate, basic chromium sulfate, chromic acid, a bichromate or the like is used, it is impossible to obtain a catalyst of high activity and performance even if ammonia is used as a precipitant.

On the other hand, use of a caustic alkali such as caustic soda or caustic potassium or an alkali carbonate such as sodium carbonate or sodium bicarbonate as a precipitant makes it impossible to obtain any highly-active catalyst even if chromium nitrate or chromium chloride is used.

Similarly, it is impossible to obtain a highly-active catalyst from chromium oxide which has been obtained by subjecting chromium nitrate, chromic anhydride or commercial chromium hydroxide to pyrolysis.

It is preferable to maintain the calcination temperature of the catalyst at a level lower than 800°C. If a catalyst is calcined at a temperature of 800°C or higher, its catalytic activity may be 5 reduced sharply.

Although no particular limitation is imposed on the lower limit of the calcination temperature, it is generally preferable to effect its calcination at least at a temperature where the oxidation reaction of 10 hydrogen chloride is carried out.

In many instances, the calcination is conducted by loading the dried precipitate in a separate calcination furnace. However, the calcination treatment may also be effected simultaneously with the 15 reaction in a tubular reactor employed for the reaction.

The following methods may be followed to prepare the catalyst composed of the chromium compound and silicon compound. (1) A silicon compound, e.g., ethyl 20 silicate is mixed in advance in an aqueous solution of the above-mentioned chromium salt. The resultant aqueous mixture is then reacted with ammonia, whereby chromium hydroxide and silicon hydroxide are co-precipitated. (2) Silica sol is mixed to an aqueous 25 solution of the aforementioned chromium salt, followed by an addition of ammonia to form a precipitate. (3)

The precipitate obtained from the above-mentioned chromium salt and ammonia is mixed and kneaded with a silica sol such as colloidal silica or fine silica particles in the presence of water. The thus-kneaded 5 mass is air-dried at room temperature in a usual manner, dried at 80 - 120°C and then calcined into a catalyst. The mixed slurry of the chromium precipitate and the silicon compound may be formed into fine spherical particles and then dried in a spray drier. 10 They may then be calcined to obtain a catalyst suitable for use in a fluidized bed. A mixed paste of the chromium precipitate and silicon compound may be extruded, dried and then calcined to obtain a catalyst suitable for use in a fixed bed. 15 As a still further alternative, the above-mentioned compound obtained in the reaction of the chromium salt and ammonia may be washed, dried and optionally calcined. It may then be mixed with a silicon compound, for example, silica sol, silica gel, 20 a silicic acid ester or the like. The resulting mixture may then be dried and optionally calcined again to obtain a catalyst. Here, the chromium and silicon compounds may be formed into a mixed slurry, which is then dried by spray drier. The resultant catalyst is 25 suitable for use in a fluidized bed. On the other hand, the mixture of the chromium compound and silicon

compound may be extruded to form a catalyst suitable for use in a fixed bed.

No particular limitation is generally imposed on the mixing ratio of chromium to silica. Expressing it 5 in terms of the weight ratio of Cr_2O_3 to SiO_2 in the final product obtained eventually subsequent to the calcination of each catalyst, $\text{Cr}_2\text{O}_3/\text{SiO}_2$ may often range from 30/70 to 95/5.

The principal effect, which can be brought about 10 from the addition of silica, resides in an increase to the mechanical strength of a catalyst, particularly, in an increase to the attrition resistance of a catalyst which has been formed into fine particles for use in a fluidized bed.

15 When chromic anhydride is used as a starting material for the catalyst, a catalyst is prepared by reacting chromic anhydride with hydrogen chloride in the following manner and then reacting the resultant reaction mixture further with ammonia in such a manner 20 as mentioned above.

The reaction is carried out by adding and reacting chromic anhydride CrO_3 to an aqueous solution of hydrochloric acid or blowing hydrogen chloride gas into an aqueous solution of chromic anhydride dissolved in water. The reaction between 25 chromic anhydride and hydrogen chloride is suitably effected

in a temperature range of from room temperature to 100°C. As to the proportions of chromic anhydride and hydrogen chloride to be required, hydrogen chloride may generally be used in an amount of 6 - 20 moles as HCl per mole of CrO₃. The time required for the reaction may range from 10 minutes to 20 hours.

Ammonia is thereafter added into the above-described aqueous solution, whereby the pH of the aqueous solution is brought to the vicinity of the neutral level to precipitate a chromium compound. The thus-obtained precipitate is treated in the same manner as the above-mentioned process either as is or as a mixture with a silicon compound.

According to the process of this invention, it is possible to treat hydrogen chloride in a volume much greater than conventional processes, namely, an hourly HCl space velocity of 700 - 1800 hr⁻¹ at a temperature lower than those employed in the conventional processes, namely, at a temperature of 300 - 360°C or so. Moreover, the thus-achieved conversion reaches 100% of the equilibrium conversion. In other words, the present invention can achieve a high conversion of hydrogen chloride at a volume rate much higher than any conventionally-known catalyst systems. Therefore, the present invention has provided an industrially-advantageous production

process of chlorine, which permits efficient production of chlorine from hydrogen chloride.

The present invention will hereinafter be described by the following Examples.

5 Example 1:

Dissolved in 3 l of deionized water was 300 g of chromium nitrate nonahydrate. While thoroughly stirring the resultant solution, 285 g of 28% aqueous solution of ammonia was added dropwise over 10 minutes.

10 The resultant slurry of precipitate was added with deionized water to dilute it to 20 l. After allowing the resultant mixture to stand overnight, it was subjected to repeated decantation to wash the precipitate. The precipitate was collected by 15 filtration and air-dried. After drying the precipitate at 100 - 120°C for 6 hours, it was heated from 100 - 600°C in the course of 3 hours and then calcined at 550°C for 4 hours in an electric furnace.

After the calcination, the catalyst was crushed.

20 Fifteen grams of beads which had diameters in the range of 1 - 1.5 mm were packed in a reactor having an inner diameter of 1 inch and made of stainless steel and then externally heated to 340°C in a fluidized sand bath.

25 At flow velocities of 200 ml/min. and 360 ml/min. (SV = 2,280 hr⁻¹), hydrogen chloride gas and

air were respectively preheated to 300°C and then introduced in the catalyst layer to react them to each other.

The reactor off-gas was caught by a trap which 5 consisted of an absorption bottle of an aqueous solution of potassium iodide and another absorption bottle of an aqueous solution of caustic soda, said bottles being connected in series. The aqueous solutions were titrated with sodium thiosulfate and 10 hydrochloric acid to quantitatively analyze the unreacted hydrogen chloride and the resultant chlorine. The conversion of hydrogen chloride was 81%, which was equivalent to 100% of the equilibrium conversion at the above reaction temperature.

15 Example 2:

Dissolved in 3 l of deionized water was 200 g of chromium chloride hexahydrate. While thoroughly stirring the resultant solution, 290 g of 28% aqueous solution was added dropwise to form a precipitate. The 20 resultant slurry of the precipitate was added with deionized water to dilute it to 20 l. After allowing the resultant mixture to stand overnight, it was subjected to decantation to wash the precipitate. The precipitate was collected by filtration.

25 After air-drying the thus-collected precipitate, it was dried at 100°C for 6 hours, heated to 550°C in

the course of 3 hours and then calcined at 550°C for 4 hours in an electric furnace to prepare a catalyst.

Fifteen grams of the above catalyst were packed in an apparatus similar to that employed in Example 1.

5 At a catalyst bed temperature of 355°C, hydrogen chloride and air were introduced respectively at flow velocities of 100 ml/min. and 185 ml/min. for their reaction. Chlorine occurred with a conversion of 70% based on the hydrogen chloride. The conversion was a 10 value corresponding to 90% of the equilibrium conversion.

Example 3:

After a precipitate slurry obtained from chromium nitrate and aqueous ammonium in a manner 15 similar to that in Example 1 was washed by decantation, the slurry was dried in a spray drier to obtain particulate powder. In a fluidized calcination furnace, the powder was calcined at 600°C for 3 hours in a fluidized state while feeding air. A fraction of 20 the catalyst, which fraction ranges from 100 - 150 mesh in particle size, was collected by sieving. Sixty grams of the catalyst fraction were packed in a fluidized-bed reactor having an inner diameter of 40 mm. The catalyst was externally heated to 340°C in an 25 electric furnace. Hydrogen chloride gas, oxygen gas and nitrogen gas were introduced respectively at 800

ml/min., 296 ml/min. and 300 ml/min. into the catalyst bed. While maintaining the catalyst in a fluidized state, the reactant gases were reacted. Chlorine gas was produced with a conversion of 76% based on hydrogen chloride.

5 Example 4:

After drying at 110°C a precipitate which had been obtained in the same manner as in Example 1, the calcination temperature was changed to 400°C, 500°C, 10 600°C, 700°C, 800°C and 900°C to prepare 6 catalysts of different types. The calcination time was each 3.5 hours. In the same apparatus and method as those employed in Example 1, the reactant gases were reacted at 350°C. Results are summarized in Table 1.

15

Table 1

Calcination temperature (°C)	400	500	600	700	800	900
Conversion of hydrogen chloride (%)	82	81	77	72	60	32

Comparative Examples 1 - 5:

20 Catalysts were prepared by changing the starting material for chromium and precipitant in various ways. Reactions were carried out in an apparatus and

precipitant similar to those employed in Example 1.

Results are summarized in Table 2.

Incidentally, hydrogen chloride gas and air were fed at 400 Ni/kgCat·hr and 720 Ni/kgCat·hr respectively.

Table 2

Comp. Ex. No.	Chromium source	Preci- pitant	Conversion of hydrogen chloride
1	chromium sulfate	ammonia	31%
2	basic chromium sulfate	ammonia	25%
3	chromium acetate	ammonia	28%
4	potassium bicarbonate + HCl	ammonia	38%
5	chromium nitrate	caustic soda	35%
6	chromium chloride	caustic soda	28%

Comparative Examples 6 - 12:

Using catalysts obtained respectively by subjecting chromium nitrate, chromic anhydride, ammonium chromate and commercial chromium hydroxide to pyrolysis and then calcining the resultant pyrolysates at 500°C, reactions were respectively carried out in the same apparatus and under the same conditions as

those employed in Example 1. Results are shown in Table 3. Furthermore, silica gel beads having a surface area of $150 \text{ m}^2/\text{g}$ and an average pore diameter of 100 \AA were impregnated with an aqueous solution of chromium chloride. The thus-impregnated silica gel beads were dried and then calcined at 400°C . Results obtained respectively by using the thus-obtained catalyst and commercial chromium oxide catalysts ("X-421", trade name; product of Nikki Chemical Industries, Ltd.) and ("G-41", trade name; Girdler Company) are also given in Table 3.

Table 3

Comp. Ex.No.	Chromium source	Conversion of hydrogen chloride
6	chromium nitrate	25%
7	chromic anhydride	36%
8	commercial chromium hydroxide	18%
9	chromium chloride/ SiO_2	21%
10	commercial chromium oxide catalyst (X-421)	24%
11	commercial chromium oxide catalyst (G-41)	7%
12	ammonium chromate	42%

Example 5:

Dissolved in 3 l of deionized water was 300 g of chromium nitrate nonahydrate. While thoroughly stirring the resultant solution, 285 g of 28% aqueous solution was added dropwise over 15 minutes. The resultant precipitate was washed by decantation. After collecting the thus-washed precipitate by filtration and then air-drying same, it was dried at 100 - 120°C for half a day. It was then calcined at 500°C for 3 hours. The thus-obtained chromium oxide was ground into fine powder in a mortar. The powdery chromium oxide was added with 28 g of silica sol ("Snowtex", trade name; product of Nissan Chemical Industries, Ltd.), followed by a further addition of 25 g of water. The resultant mixture was kneaded. After the kneading, the resultant paste was extruded into pellets of 3 mm in diameter and 4 mm in length. After drying the pellets at 100°C, they were calcined at 550°C for 4 hours to prepare a catalyst. The circumferential breaking strength of the catalyst was 3.5 - 3.8 kg. Accordingly, the catalyst shows sufficient strength as an industrial catalyst.

Fifty grams of the catalyst were packed in a reactor having an inner diameter of 1 inch and made of stainless steel and were then externally heated to 350°C in a fluidized sand bath. At flow velocities of

4.8 Nl/hr. and 90 Nl/hr., hydrogen chloride gas and air were respectively introduced into the catalyst layer to react them to each other. The reaction gas was sampled, and the unreacted hydrogen chloride and 5 the thus-produced chlorine were quantitatively analyzed: The analysis showed that chlorine was produced at a conversion of 76% based on hydrogen chloride.

Example 6:

10 Dissolved in 3 l of deionized water was 300 g of chromium nitrate nonahydrate, followed by an addition of 72 g of an ethyl silicate solution. While thoroughly stirring the resultant mixture, liquid ammonia was added dropwise to obtain a co-precipitated 15 compound of chromium hydroxide and silica hydrogel. The compound was dried by a pressurized-nozzle spray drier to obtain fine spherical beads. They were calcined at 600°C in a fluidized state to prepare a catalyst. Eighty grams of the catalyst were placed in 20 a fluidized-bed reactor having an inner diameter of 40 mm. The catalyst was externally heated to 350°C. Hydrogen chloride and oxygen were introduced respectively at 55 Nl/hr. and 25 Nl/hr. into the catalyst bed for their reaction. Chlorine was produced 25 at a conversion of 81% based on the hydrogen chloride.

Example 7:

Dissolved in 3 l of deionized water was 300 g of chromium nitrate nonahydrate, followed by a dropwise addition of 28% aqueous ammonia to cause chromium hydroxide to precipitate. The thus-obtained precipitate was collected by filtration, to which 200 g of silica sol ("Snowtex", trade name; product of Nissan Chemical Industries, Ltd.) was added. They were mixed thoroughly into a slurry. The slurry was then dried in a spray drier to convert it into fine spherical beads. They were then calcined at 500°C in a fluidized state to prepare a catalyst. Using the the catalyst, hydrogen chloride and oxygen were reacted under the same conditions as in Example 6, thereby achieving a conversion of 79% based on the hydrogen chloride.

Example 8:

Dissolved in 3 l of deionized water was 300 g of chromium nitrate nonahydrate, followed by a dropwise addition of 28% aqueous ammonia to cause chromium hydroxide to precipitate. After washing, filtering and drying the precipitate, the precipitate was calcined at 400°C for 3 hours to convert it into chromium oxide and the chromium oxide was ground into particles of 100 mesh and smaller.

The above-obtained powder was added with 50 g of silica sol ("Snowtex", trade mark; product of Nissan

Chemical Industries, Ltd.) and 15 g of water. They were thoroughly mixed and kneaded in a kneader. The resulting paste was extrusion into pellets of 3 mm in diameter and 4 mm in length. They were dried and then 5 calcined at 550°C for 4 hours, thereby preparing a catalyst:

Using the the catalyst, hydrogen chloride and oxygen were reacted under the same conditions as in Example 5, thereby achieving a conversion of 79% based 10 on the hydrogen chloride.

Examples 9 - 15:

Changing the starting catalyst raw material in various ways, chromia-silica catalysts were prepared in accordance with the procedure of Example 5. Reactions 15 were conducted in the same manner as in Example 5, using the above-mentioned chromia-silica catalysts respectively. Reaction results are summarized in Table 4.

Table 4

20

Comp. Ex.No.	Chromium source	Preci- pitant	Conversion of hydrogen chloride
9	chromium nitrate	NaOH	23%
10	chromium nitrate	KOH	19%
11	chromium sulfate	aqueous ammonia	20%

Table 4 (Cont'd)

Comp. Ex. No.	Chromium source	Preci- pitant	Conversion of hydrogen chloride
5	chromium alum	aqueous ammonia	17%
	chromium chloride	aqueous ammonia	68%
	chromium acetate	aqueous ammonia	74%
	chromium propionate	aqueous ammonia	70%

Example 16:

Catalysts were obtained by calcining portions of a chromia-silica catalyst, which had been obtained in the same manner as in Example 5, at various calcination temperatures. Their activities were measured. The reaction conditions were the same as those employed in Example 5. Results are given in Table 5.

Table 5

15	Calcination temperature (°C)	350	400	500	600	700	800	900
	Conversion of hydrogen chloride (%)	76	78	77	77	70	53	31

Example 17:

A precipitate, which had been obtained by adding aqueous ammonia to an aqueous solution of chromium nitrate, was collected in the form of a slurry by 5 filtration. The slurry was mixed with silica sol in such an amount that the weight ratio of Cr_2O_3 to SiO_2 became 1:1. The resultant mixture was continuously stirred for 3 hours to obtain a homogeneous slurry. This slurry was dried in a spray 10 drier and then calcined at 500°C to prepare a fine spherical catalyst for use in a fluidized bed. Under the same reaction conditions as those employed in Example 6, its catalytic activity was measured. As a 15 result, chlorine was produced at a conversion of 73% based on hydrogen chloride.

Example 18:

Five hundred grams of chromic anhydride were added to and dissolved in 3 l of 35% hydrochloric acid. They were reacted at 65°C for 1 hour with 20 stirring. After completion of the reaction, nitrogen gas was bubbled at 70°C for 10 minutes through the reaction mixture. The thus-treated reaction mixture was allowed to cool down, to which deionized water was added to dilute same to a total volume of 6 l. With 25 thorough stirring, 1.9 l of 28% aqueous ammonia was added over 3 hours.

The thus-formed precipitate was collected by filtration and was then washed. It was then converted into a paste-like form by a kneader, followed by its extrusion. After drying the extrudates at 100°C for 5 hours, they were calcined at 250°C for 3 hours and then at 600°C for additional 3 hours to prepare a tablet-like catalyst of 4 mm in diameter and 5 mm in height.

One hundred grams of the catalyst was packed in a reactor having an inner diameter of 1 inch and made of Hastelloy-C. The catalyst bed was externally heated to 340°C in a fluidized sand bath. A gaseous mixture of 80 l/hr. of hydrogen chloride gas and 30 l hr. of oxygen was fed to the reactor. Chlorine in the resultant gas was analyzed. Chlorine was produced at a conversion of 80% based on the hydrogen chloride.

Example 19:

Five hundred grams of chromic anhydride were added to and dissolved in 3 l of 35% hydrochloric acid. They were reacted at 70°C for 30 minutes with stirring. After completion of the reaction, air was bubbled at 70°C for 10 minutes through the reaction mixture. The thus-treated reaction mixture was allowed to cool down, to which deionized water was added to dilute same to a total volume of 7 l. With thorough

stirring, 1.9 l of 28% aqueous ammonia was added over 3 hours.

The thus-formed precipitate was washed with water and then collected by filtration. It was then 5 added with 750 g of silica sol (SiO_2 content: 20 wt.%) and the resultant mixture was thoroughly stirred into a homogeneous slurry. After adjusting the concentration of the slurry to about 6.5%, it was dried and formed into small particles in a spray drier. The 10 particles were thereafter calcined at 250°C for 2 hrs. and then at 600°C for 3 hours in air, thereby preparing a fine particulate catalyst suitable for use in a fluidized bed. The catalyst had an average particle size of 65 μm and a packing density of 1.2. 15 Fine particles having good attrition resistance were obtained.

In a fluidized-bed reactor having an inner diameter of 2 inches, 350 g of the catalyst was packed. 20 Into the catalyst bed, hydrogen chloride and oxygen were introduced respectively at 240 l/hr. and 90 l hr. under a total pressure of 3 kg/cm^2 . The reactor was externally heated to 340°C to react the hydrogen chloride and oxygen. Chlorine was produced at a conversion of 78% based on the hydrogen chloride.

CLAIMS

1. A process for producing chlorine by oxidizing hydrogen chloride with an oxygen-containing gas, which comprises 5 effecting the oxidation in the presence of a catalyst prepared from a chromium compound which has been obtained by reacting chromium nitrate, chromium chloride or the chromium salt of an organic acid with ammonia.
- 10 2. A process for producing chlorine by oxidizing hydrogen chloride with an oxygen-containing gas, which comprises effecting the oxidation in the presence of a catalyst prepared from a chromium compound which has been obtained by reacting chromic anhydride with an aqueous solution of 15 hydrochloric acid and then reacting the resultant aqueous reaction mixture with ammonia.
- 20 3. A process of claim 1 or claim 2, wherein the catalyst has been prepared from a mixture of the chromium compound and a silicon compound.
4. A process as claimed in any one of claims 1, 2 and 3, wherein upon preparation of the catalyst, the catalyst is calcined at a temperature lower than 800°C.
- 25 5. A process for producing chlorine by oxidizing hydrogen chloride with an oxygen-containing gas, which comprises

effecting the oxidation in the presence of a catalyst prepared from a chromium compound, which has been obtained by reacting a chromium salt with ammonia, and a silicon compound.

5

6. A process as claimed in claim 5, wherein the catalyst has been obtained by calcining a mixture of a chromium compound, which was obtained by reacting chromium nitrate, chromium chloride or the chromium salt of an organic acid 10 with ammonia, and the silicon compound at a temperature lower than 800°C.

7. A process as claimed in claim 5, wherein the catalyst is a mixture of a material which has been obtained by 15 reacting chromium nitrate, chromium chloride or the chromium salt of an organic acid with ammonia and then calcining the resultant chromium compound at a temperature lower than 800°C, and a silicon compound.

20 8. A process as claimed in claim 5, wherein the catalyst has been obtained by calcining a mixture of a material, which was obtained by reacting chromium nitrate, chromium chloride or the chromium salt of an organic acid with ammonia and then calcining the resultant chromium compound 25 at a temperature lower than 800°C, and a silicon compound further at a temperature lower than 800°C.

9. A process of any one of the preceding claims, wherein the oxygen-containing gas is oxygen gas or air.

10. A process of any one of the preceding claims, wherein
5 the catalyst comprises the chromium compound and a silicon compound corresponding to a $\text{Cr}_2\text{O}_3/\text{SiO}_2$ weight ratio in the range of 30/70 - 95/5.

11. A process of any one of the preceding claims, wherein
10 the molar ratio of oxygen to hydrogen chloride to be reacted (O_2/HCl) is in the range of 0.2 - 1.

12. A process of any one of the preceding claims, wherein
the oxidation is effected at a temperature of 300°C - 450°C.
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13. A process of any one of the preceding claims, wherein
the oxidation is effected at a pressure of atmospheric
pressure - 10 kg/cm²G.